



Universidad de Valladolid

Metrología para la descarbonización de la red de gas

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Ávila, del 27 al 29 de septiembre de 2022



Outline

- **TermoCal**
- Motivation
- Low-carbon gas networks
 - Decarb
 - Accurate Thermophysics
- Discussion



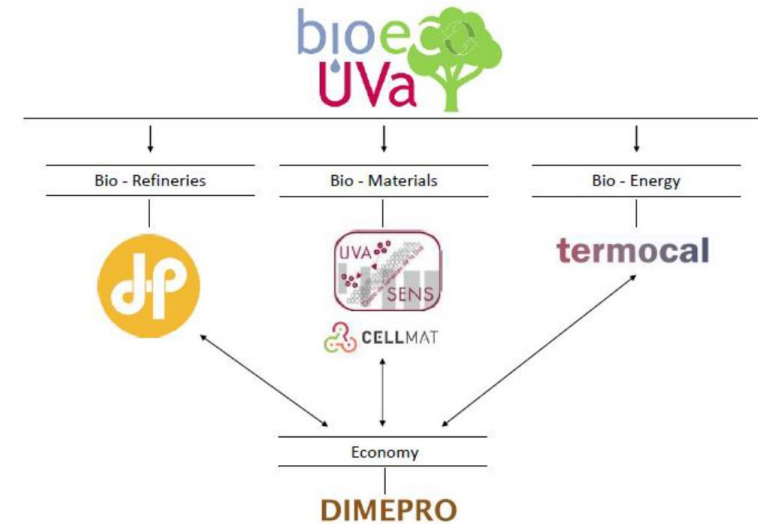
TermoCal
University of Valladolid
Thermophysics & Calibration



- 1) **Fundamental Metrology**
- 2) **Thermophysical Properties and Phase Behaviour** of multicomponent fluid mixtures over wide ranges of temperatures, pressures and chemical compositions
- 3) **Exergy analysis** of systems and processes



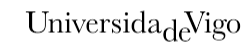
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Technique	Property	Temperatures	Maximum Pressure	Uncertainty*
Single-sinker Magnetic Suspension Densimeter	Gas Density	(250 to 400) K	20 MPa	(0.02 to 0.4) %
Spherical Acoustic Resonator	Speed of Sound in Gases	(200 to 475) K	20 MPa	0.02 %
Flow Calorimeter	Isobaric Heat Capacity	(240 to 420) K	25 MPa	0.4 %
Vibrating Tube Densimeter	Density	(240 to 420) K	140 MPa	0.1 %
Flow Calorimeter	Excess Enthalpy	(240 to 420) K	25 MPa	1.0 %
Falling Body Viscometer	Viscosity	(240 to 475) K	140 MPa	3 %
Vibrating Wire Viscometer	Viscosity	(200 to 475) K	140 MPa	1.5 %
Static Isochoric Total Pressure VLE Cell (Van Ness)	Phase Equilibrium	(240 to 400) K	10 MPa	0.001 in liquid mole fraction
Cylindrical Microwave Resonator	Phase Equilibrium	(200 to 360) K	50 MPa	0.1 % in pressure

* Overall Expanded Uncertainty (k =2)





Competitive EU Projects



MetCCUS



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Natural gas is currently the primary source of energy for heat in Europe and to meet climate change targets we need to quickly introduce **biomethane, hydrogen enriched natural gas, 100% hydrogen, and CCS technologies.**

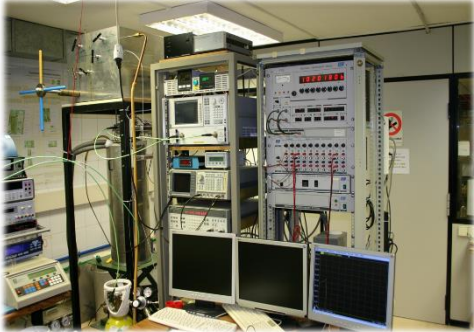


Metrology for
decarbonising
the gas grid



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Spherical Acoustic Resonator



(200 to 475) K

20 MPa



$$U(T) (k = 2) = 2.0 \cdot 10^{-3} \text{ K}$$

$$(0 - 3) \text{ MPa: } U(p)/\text{MPa} (k = 2) = 60 \cdot 10^{-6} \cdot p/\text{MPa} + 0.6 \cdot 10^{-3}$$

$$(3 - 20) \text{ MPa: } U(p)/\text{MPa} (k = 2) = 60 \cdot 10^{-6} \cdot p/\text{MPa} + 1.0 \cdot 10^{-3}$$

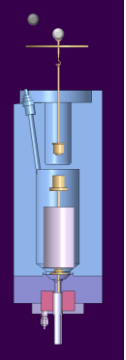
$$U_r(w) (k = 2) = 2.2 \cdot 10^{-4} \cdot \text{m} \cdot \text{s}^{-1} / \text{m} \cdot \text{s}^{-1} \quad U_r(c_p) (k = 2) = 1 \cdot 10^{-3}$$

Single Sinker Magnetic Suspension Densimeter



(250 to 400) K

20 MPa



$$U(T) (k = 2) = 4.0 \cdot 10^{-3} \text{ K}$$

$$(0 - 3) \text{ MPa: } U(p)/\text{MPa} (k = 2) = 60 \cdot 10^{-6} \cdot p/\text{MPa} + 1.7 \cdot 10^{-3}$$

$$(3 - 20) \text{ MPa: } U(p)/\text{MPa} (k = 2) = 75 \cdot 10^{-6} \cdot p/\text{MPa} + 3.5 \cdot 10^{-3}$$

$$U(\rho)/\text{kg} \cdot \text{m}^{-3} (k = 2) = 1.1 \cdot 10^{-4} \cdot \rho/\text{kg} \cdot \text{m}^{-3} + 2.3 \cdot 10^{-2}$$

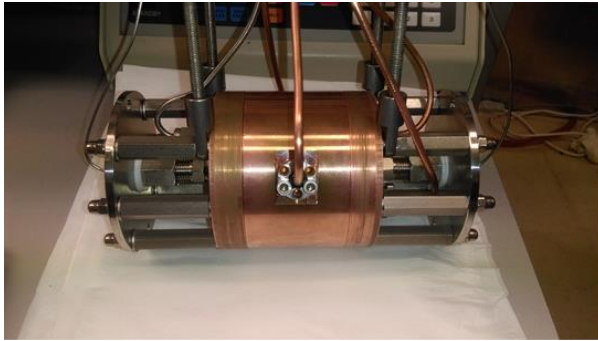
WP3. 3.1.1; 3.1.3; 3.1.4 (ρ and w of H_2 and alkane binary mixtures)

$$250 < T/\text{K} < 330 \quad p < 12 \text{ MPa}$$

$\text{H}_2 + \text{C}_3\text{H}_8$ and $\text{H}_2 + \text{C}_4\text{H}_{10}$ (25, 50, 75)%

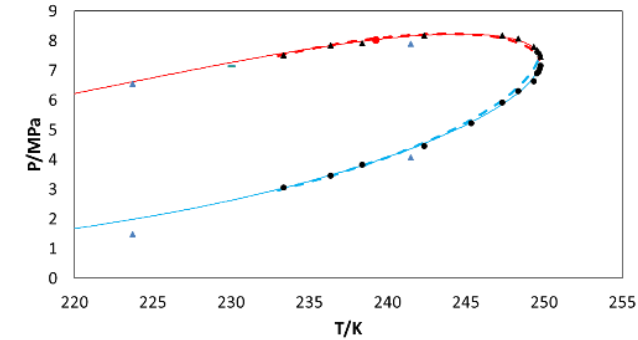
$$U_r(w) = 0.02 \% \quad U_r(\rho) = 0.05 \%$$

MW Cavities (TU-CH, UVa)



(230 to 340) K

10 MPa



$$U(T) (k = 2) = 20 \cdot 10^{-3} \text{ K}$$

$$(0 - 3) \text{ MPa: } U(p)/\text{MPa} (k = 2) = 200 \cdot 10^{-6} \cdot p/\text{MPa} + 6 \cdot 10^{-3}$$

$$(3 - 20) \text{ MPa: } U(p)/\text{MPa} (k = 2) = 200 \cdot 10^{-6} \cdot p/\text{MPa} + 10 \cdot 10^{-3}$$

$$0.0010 < U(x) (k = 2) \text{ mol} \cdot \text{mol}^{-1} < 0.010$$

WP3. Task 3.2

VLE Vapour liquid equilibrium of hydrogen and alkane binary mixtures



H₂ Impurities (H₂O): Accurate Thermophysics. *f*

Quasi-Spherical MW Resonator

$$200 \text{ K} < T < 400 \text{ K}$$

$$p < 3 \text{ MPa}$$

$$U_r(p) = 0.015\%$$

$$U(T) = 4 \text{ mK}$$

$$U_r(x_w) = 2\%$$

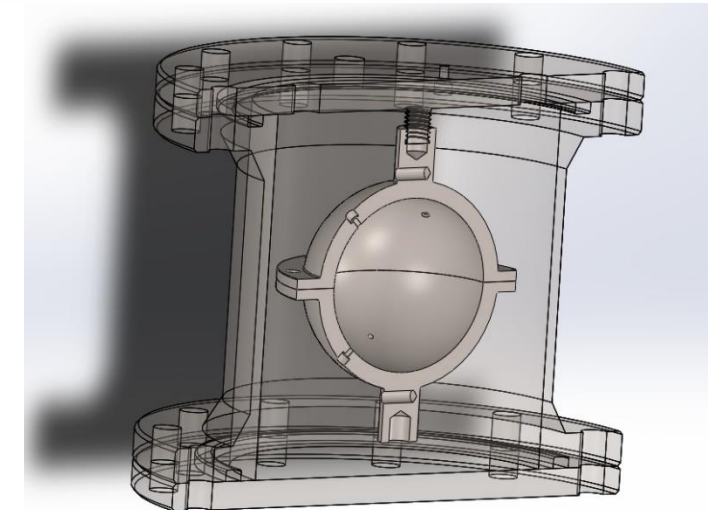
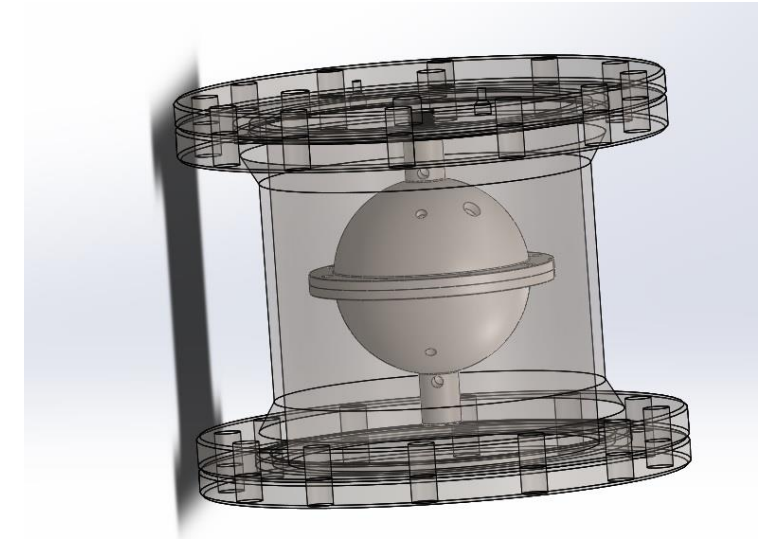
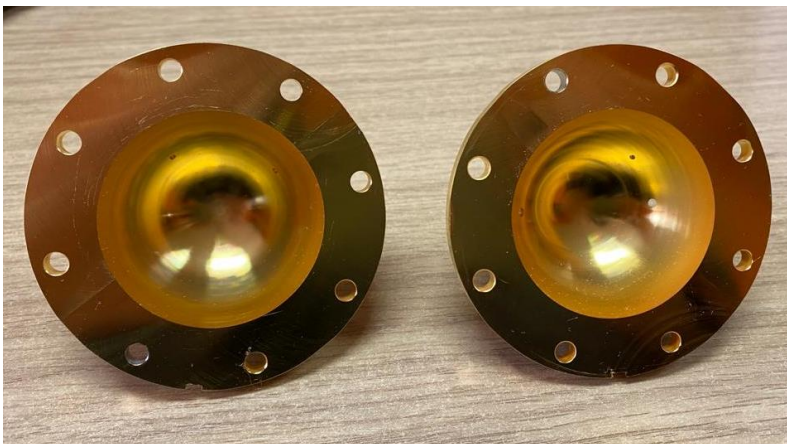
$$k = 2$$



$$D_x = 50.08 \text{ mm}$$

$$D_y = 50.16 \text{ mm}$$

$$D_z = 50 \text{ mm}$$





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Q & A

David Vega-Maza

28/09/2022



$$X_w \cdot T_{DP}$$

$$x_w = \frac{\left(\frac{\varepsilon_{mix} - 1}{\varepsilon_{mix} + 2} \frac{\varepsilon_{dry} + 2}{\varepsilon_{dry} - 1} \right) - 1}{\rho_w / \rho_{dry} - 1}$$

$$\varepsilon_{mix}(p, T) = \varepsilon_{dry}(p, T) \left(\frac{f_{dry}(p, T)}{f_{mix}(p, T)} \right)^2$$

$$\rho_{mix}(p, T) = \frac{1}{\rho_{mix}} \frac{\varepsilon_{mix} - 1}{\varepsilon_{mix} + 2}$$

$$\rho_{dry}(p, T) = \frac{1}{\rho_{dry}} \frac{\varepsilon_{dry} - 1}{\varepsilon_{dry} + 2}$$

$$\rho_{mix} = \rho_w x_w + (1 - x_w) \rho_{dry}$$